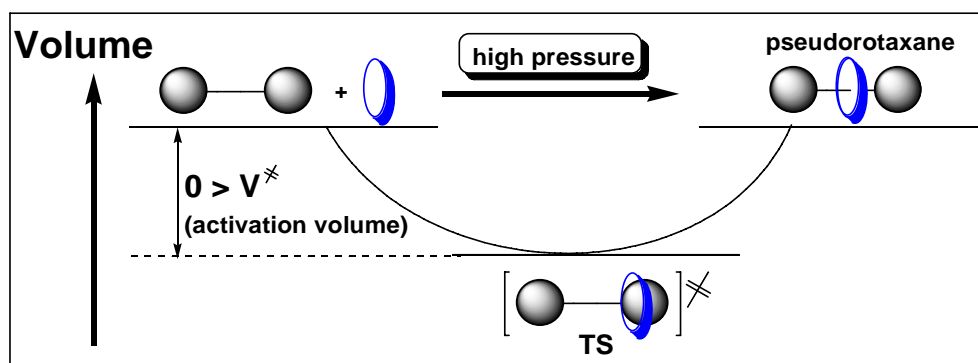


A molecular switch based on acid and base promoted, cation governed binding in a crown ether threaded rotaxane

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# Graphical Abstract



# The effect of pressure on pseudorotaxane formation by using the slipping method

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**Abstract-**By using high-pressure conditions the formation of pseudorotaxane via the slipping approach is accelerated. Analysis of the effects of pressure on the rate constants affords activation volumes for the pseudorotaxane forming, slipping reactions.

Rotaxane synthesis remains a great challenge in supramolecular chemistry.<sup>1</sup> The three main approaches used for rotaxane synthesis are the threading-stoppering,<sup>2</sup> clipping,<sup>3</sup> and slipping<sup>4</sup> methods, and others have been devised.<sup>5,6,7</sup> Among these strategies, the advantages of slipping method are that only thermal conditions are required, that other chemicals or reagents are not needed, and that by-products are not formed. Despite these advantages, only a few examples employing this technique have been reported. The major reason for this is that the stopper of the dumbbell-like axle and the cavity size of macrocycle must be designed to be rigorously complimentary, making synthesis of stable rotaxanes by this approach difficult.

High pressure reaction conditions have been used advantageously in the preparation of organic compounds that are difficult to synthesize at ambient pressures.<sup>8</sup> In general, reactions in which the molecularity decreases in proceeding from reactants to products (*e.g.*, cycloadditions and condensations) are facilitated by using high-pressures, since these processes have negative volumes of activation. Since molecularity decreases and bulky stopper part of the dumbbell-like axles must enter the cavity of hosts in the slipping synthesis of rotaxanes, it seems likely that the volumes of activation of these processes would be negative. This proposal was tested by probing the effect of pressure on the rates of formation of pseudorotaxane, comprised of secondary ammonium ions and crown ethers, by the slipping method (Fig. 1).<sup>9</sup> The results of this effort are presented below.

### Fig. 1

Kinetic measurements were made initially by using a mixture of dibenzo[24]crown8 **1a** and bis(cyclohexylmethyl)ammonium salt **2a**, a pair known to form the corresponding pseudorotaxane **3a** slowly at ambient temperature and pressure (Fig. 2).<sup>10</sup> The progress of the reaction of an equimolar (15 mM) mixture of **1a** and **2a** in CDCl<sub>3</sub>-CD<sub>3</sub>CN was monitored by using <sup>1</sup>H NMR spectroscopy. A plot of the reciprocal of the **1a** concentration *vs.* time was linear at low conversions.<sup>11,12</sup> As expected, this process shows typical second-order behaviour at conversions lower than 10%. At this point, effects of the reverse reaction of pseudorotaxane **3a** begin to contribute. Having obtained the rate constant (*k*) for pseudorotaxane formation at 1 kgcm<sup>-2</sup>, we next evaluated the effects of pressure on the rate of this process. Reactions, using equimolar mixtures (15 mM) of **1a** and **2a** in CDCl<sub>3</sub>-CD<sub>3</sub>CN) were carried out at 30 °C at pressures ranging from 1 to 5000 kgcm<sup>-2</sup>. In each case plots of 1/[**2a**] *vs.* time at low conversion were linear and gave rise to second order rate constants *k*.<sup>11</sup> As expected, the rates of rotaxane formation increase as the pressure increases. For example the rate constant at 5000 kgcm<sup>-2</sup> ( $6.5 \times 10^{-4} \pm 0.5 \times 10^{-4} \text{ M}^{-1}\text{h}^{-1}$ ) is more than 20 times larger than the value at 1 kgcm<sup>-2</sup> ( $3.3 \times 10^{-5} \pm 0.3 \times 10^{-5} \text{ M}^{-1}\text{h}^{-1}$ ) (Fig. 3). Measurements of rate constants as a function of pressure, made on pseudorotaxane forming reactions carried out at 40 and 50 °C, show that pressure increases accelerate the slipping reaction at higher temperatures also.<sup>13</sup>

**Fig. 2.**

**Fig. 3.**

Next, pressure effects on the rates of rotaxane formation between tetrabenzo[24]crown8 **1b** and dibenzylammonium salt **2b** were investigated.<sup>14</sup> These processes were conducted using 10 mM solutions (in CDCl<sub>3</sub>-CD<sub>3</sub>CN) of each reactant at 30 °C, 40 °C, and 50 °C in pressure ranges up to 3000 kgcm<sup>-2</sup>. Again, rate constants were obtained by determining the time dependence of formation of the pseudorotaxane **3b**.<sup>13</sup> The rate constants for this process are directly dependent on pressure at all temperatures ( $k(30\text{ °C}) = 1.3 \times 10^{-3} \pm 0.1 \times 10^{-3} \text{ M}^{-1}\text{h}^{-1}$  at 3000 kgcm<sup>-2</sup> and  $k(30\text{ °C}) = 1.0 \times 10^{-4} \pm 0.2 \times 10^{-4} \text{ M}^{-1}\text{h}^{-1}$  at 1 kgcm<sup>-2</sup>).<sup>15</sup>

The rate constant vs. pressure data permits an estimation of the activation volumes ( $V^\ddagger = -RT(\partial \ln k / \partial P)_T$ ) for the rotaxane forming reactions. Plots of  $\ln k$  vs.  $P$  give curved lines (Fig. 4) like those typically seen in the analysis of other high pressure-promoted reactions (*e.g.*, Diels-Alder reaction). Others have discussed how the curvature of these plots, which normally indicates that the activation volumes are not independent of pressure, complicates the accurate determination of volumes of activation difficult. A suggested solution to this problem, involving the use of the quadratic equation,  $\ln k = aP^2 + bP + c$ ,<sup>8</sup> was employed to estimate the volumes of activation for the respective **1a** + **2a** and **1b** + **2b** reactions to be -2.6 to -5.7 cm<sup>3</sup>mol<sup>-1</sup>. Although not as strongly negative as those for Diels-Alder reactions, these volumes of activation indicate that pressure can have a beneficial effect on slipping reactions used for rotaxane synthesis (Table 1).

**Fig. 4.**

**Table 1.**

Since slipping reactions are not associated with any bond cleaving and forming processes, their negative volumes of activation result from fitting the stopper end of ammonium groups into the cavity of crown in rate limiting transition states. This result suggests that free volumes in crown cavities decrease in proceeding from the reactants to the transition states for rotaxane formation as a result of the complimentary sizes of cavities and stopper ends (Fig. 5). Recently, three-dimensional structures of transition states of the slipping process were investigated by use of computational methods.<sup>16</sup> The calculated results are in good agreement with their experimental observations. The activation volumes determined in the current effort could provide a more quantitative explanation for the rigorous requirement of size complementarity in rotaxane forming, slipping reactions.

**Fig. 5**

In summary, the observations described above show that high pressures accelerate rotaxane formation by the slipping approach. Like the recently reported solventless reaction technique,<sup>17</sup> the high-pressure methodology, which leads to dramatic rate enhancements, should be applicable to a number of processes used for supramolecular self-assembly.

### Acknowledgements

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### Supplementary data

Plots of  $1/[2]$  vs. time for reactions of equimolar mixtures of **1a** with **2a** (40 and 50 °C, CDCl<sub>3</sub>-CD<sub>3</sub>CN) and of **1b** with **2b** (30, 40, and 50 °C, CDCl<sub>3</sub>-CD<sub>3</sub>CN) at various pressures.

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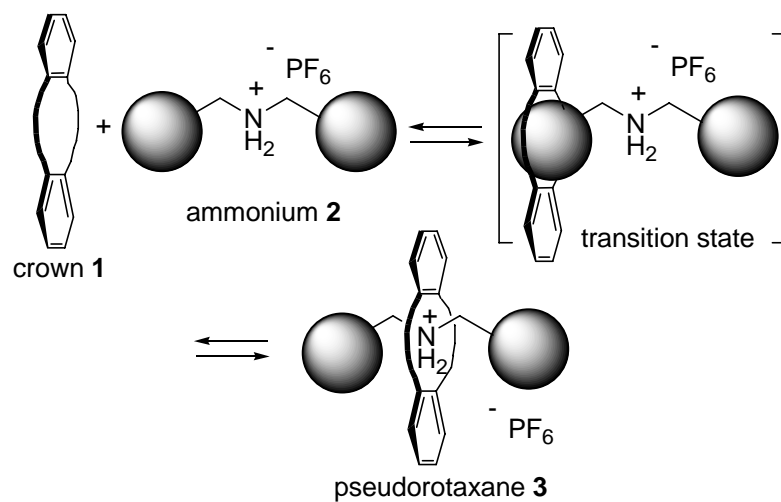
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  9. The clipping synthesis of rotaxane was employed under ultra-high-pressure, but the effect of pressure was not discussed. For example; Jeppesen, J. O.; Nielsen, K. A.; Perkins, J.; Vignon, S. A.; Fabio, A. D.; Ballardini, R.; Gandolfi, M. T.; Venturi, M.; Balzani, V.; Becher, J.; Stoddart, J. F. *Chem. Eur. J.*, **2003**, *9*, 2982-3007.
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  11. When the formation of ion-pairs was not considered, the second-order rate equation would be  

$$-d[1]/dt = -d[2]/dt = k[1][2] \quad \text{In the case of } [1] = [2]$$

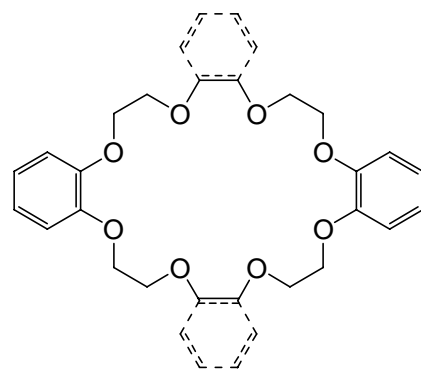
$$1/[2] = kt + 1/[2]_0$$
  12. The association constant between ammonium salts and ammonium ions using ammonium-crown system in CDCl<sub>3</sub>/CD<sub>3</sub>CN was reported by Gibson's group. In consideration of their results, ca 70% of ammonium existed as an ion during our reactions at 1 kgcm<sup>-2</sup>. Even though high-pressure condition accelerates the dissociation of ion pairing, the promotion of the slipping is less than 1.4 times; see: Jones, J. W.; Gibson, H. W. *J. Am. Chem. Soc.* **2003**, *125*, 7001-7004.
  13. See electronic supplementary data.
  14. Since TB24C8 has a delicately smaller cavity size, the association rate of **1b** and **2b** is favorable to monitor; see; Tokunaga, Y.; Goda, T.; Wakamatsu, N.; Nakata, R.; Shimomura, Y. *Heterocycles*, **2006**, *68*, 5-10.

15. The thermal reaction of both reactants (50 °C, 1 atm, 28days) afforded **3b** in 58% conversion yield. In contrast, the high-pressure conditions (50 °C, 2500atm, 17days) gave **3b** in 66% conversion yield.
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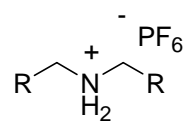




**Figure 1.** An illustration of the slipping approach for rotaxane synthesis.

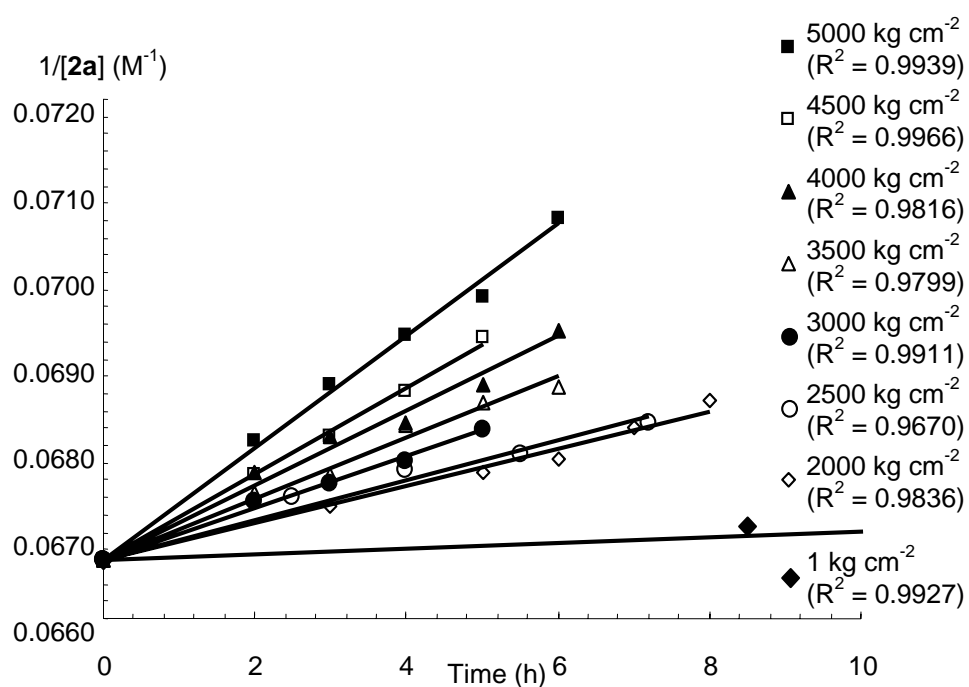


**1a:** DB24C8  
**1b:** TB24C8

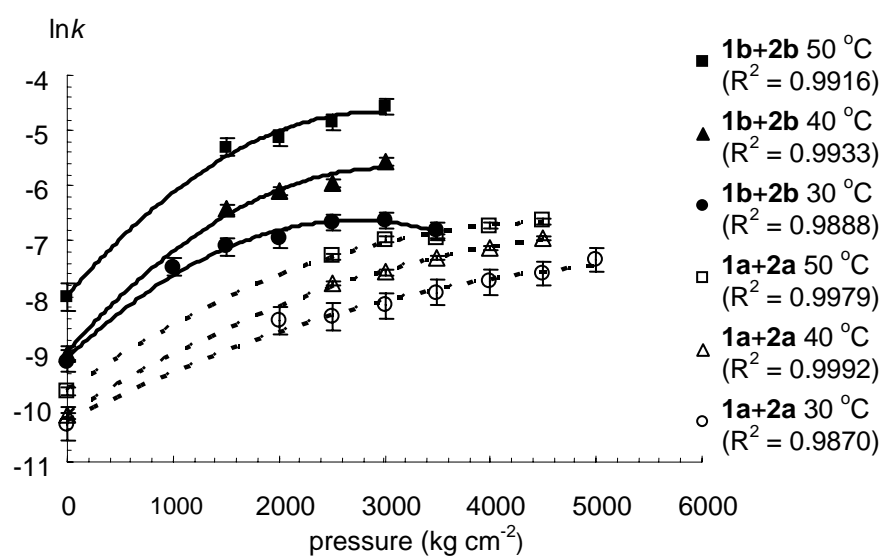


**2a:** R = C<sub>6</sub>H<sub>11</sub>  
**2b:** R = C<sub>6</sub>H<sub>5</sub>

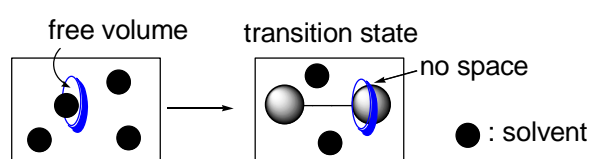
**Figure 2.** Structures of crowns **1** and ammonium salts **2**.



**Figure 3.** Plots of  $1/[2a]$  vs. time for reaction of equimolar (15 mM) mixtures of **1a** with **2a** ( $30\text{ }^{\circ}\text{C}$ ,  $\text{CDCl}_3\text{-CD}_3\text{CN}$ ) at various pressures.



**Figure 4.** Plots of  $\ln k$  vs. pressure for reactions of **1a** with **2a** (15 mM, 30 °C, CDCl<sub>3</sub>-CD<sub>3</sub>CN) and of **1b** with **2b** (10 mM, 30 °C, CDCl<sub>3</sub>-CD<sub>3</sub>CN).



**Figure 5.** A pictorial representation of rotaxane forming, slipping processes.

**Table 1.** The activation volumes of the pseudorotaxane formation at 1 kg cm<sup>-2</sup>.<sup>a</sup>

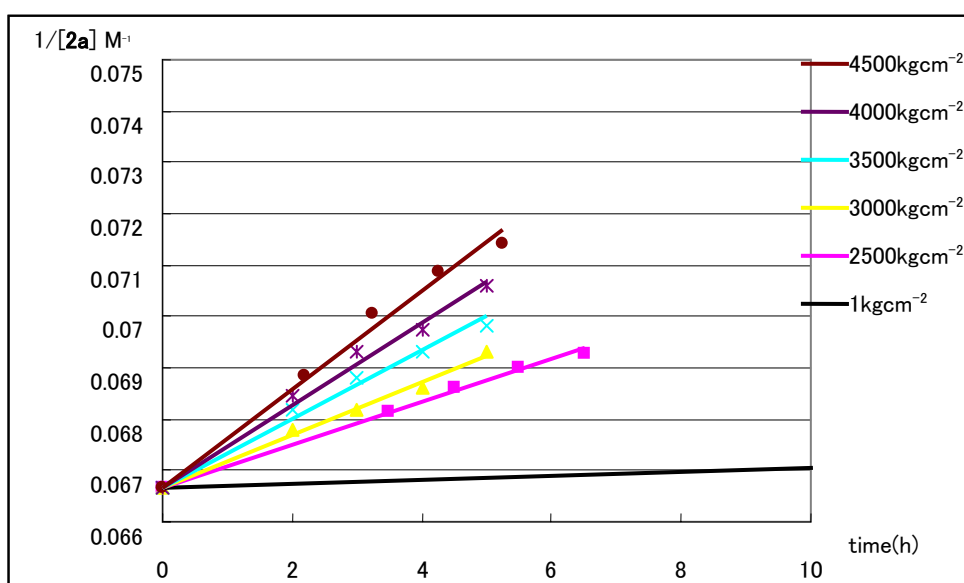
	<b>1a-2a</b>	<b>1b-2b</b>
30 °C	-2.6	-4.9
40 °C	-3.1	-5.7
50 °C	-3.4	-5.7

<sup>a</sup> cm<sup>3</sup> mol<sup>-1</sup>.

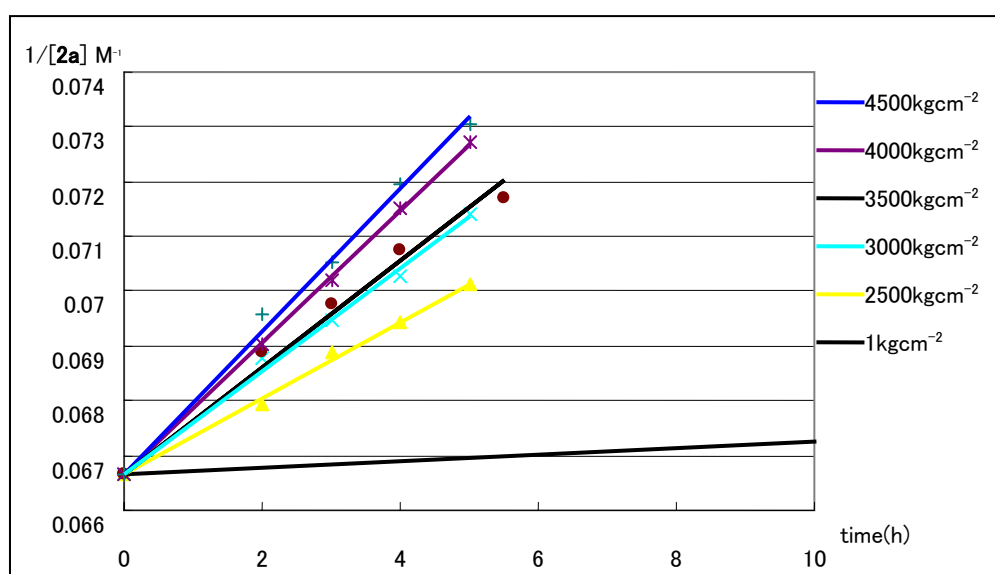
-Supplementary Data-

**Kinetics of pseudorotaxane formation**

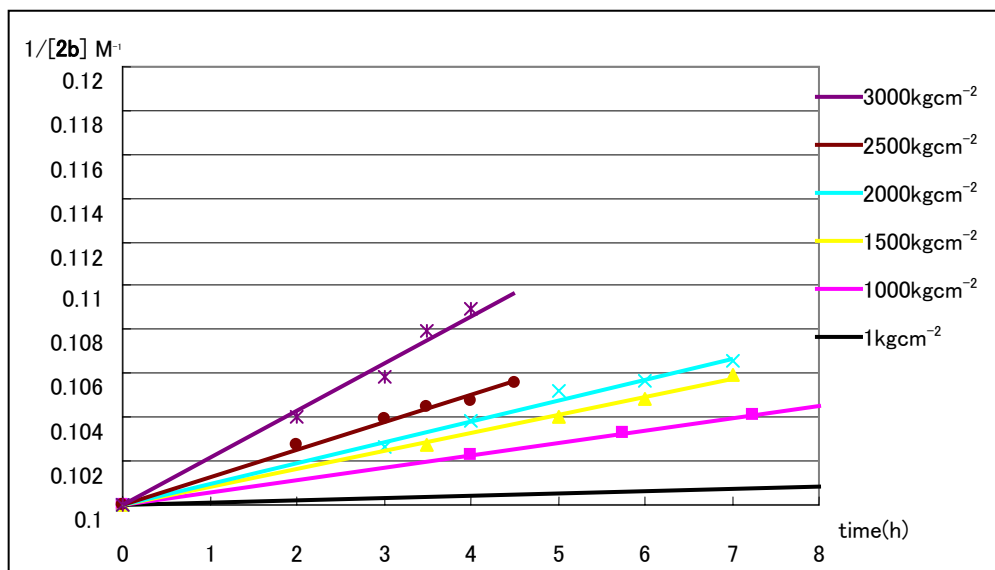
**1a-2a at 40°C**



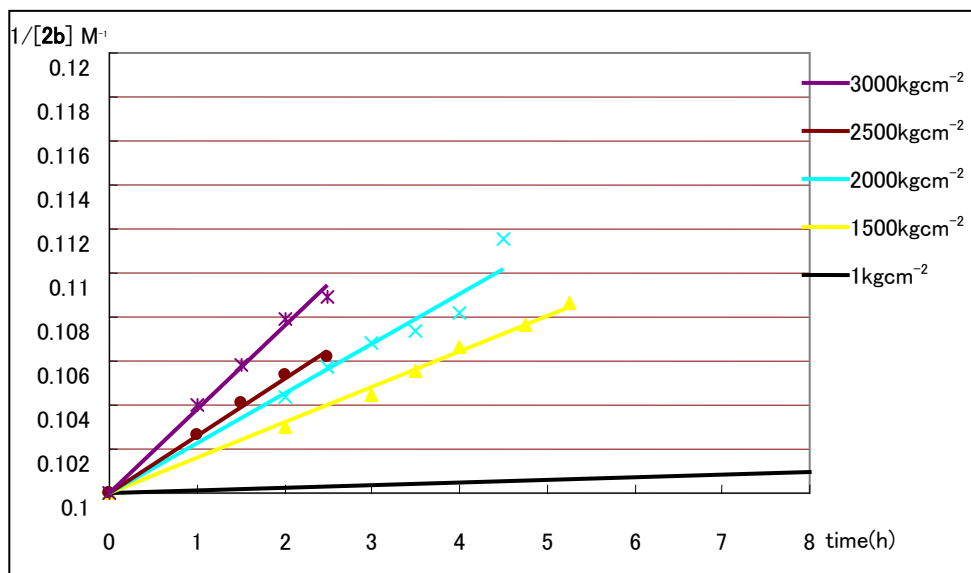
**1a-2a at 50°C**



**1b-2b at 30°C**

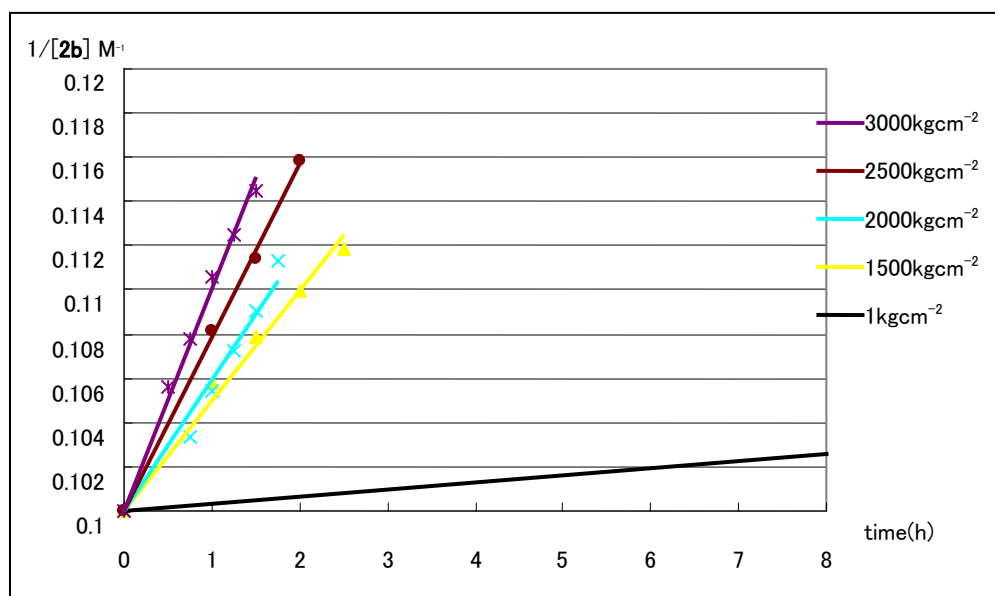


**1b-2b at 40°C**





**1b-2b at 50°C**



**Table.** The reaction constant ( $M^{-1}h^{-1}$ ) of reactions between **1** and **2**.

**1a+2a**

30°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$0.33 \times 10^{-4}$	$0.03 \times 10^{-4}$
2000	$2.2 \times 10^{-4}$	$0.20 \times 10^{-4}$
2500	$2.3 \times 10^{-4}$	$0.62 \times 10^{-4}$
3000	$2.8 \times 10^{-4}$	$0.62 \times 10^{-4}$
3500	$3.6 \times 10^{-4}$	$0.44 \times 10^{-4}$
4000	$4.3 \times 10^{-4}$	$0.72 \times 10^{-4}$
4500	$5.0 \times 10^{-4}$	$0.21 \times 10^{-4}$
5000	$6.5 \times 10^{-4}$	$0.47 \times 10^{-4}$

40°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$0.39 \times 10^{-4}$	$0.02 \times 10^{-4}$
2500	$4.2 \times 10^{-4}$	$0.52 \times 10^{-4}$
3000	$5.2 \times 10^{-4}$	$0.52 \times 10^{-4}$
3500	$6.7 \times 10^{-4}$	$1.01 \times 10^{-4}$
4000	$8.1 \times 10^{-4}$	$0.91 \times 10^{-4}$
4500	$9.6 \times 10^{-4}$	$0.77 \times 10^{-4}$

50°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$0.60 \times 10^{-4}$	$0.05 \times 10^{-4}$
2500	$7.0 \times 10^{-4}$	$0.55 \times 10^{-4}$
3000	$9.4 \times 10^{-4}$	$1.10 \times 10^{-4}$
3500	$9.7 \times 10^{-4}$	$1.30 \times 10^{-4}$
4000	$12 \times 10^{-4}$	$0.32 \times 10^{-4}$
4500	$13 \times 10^{-4}$	$1.56 \times 10^{-4}$

**1b+2b**

30°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$1.0 \times 10^{-4}$	$0.23 \times 10^{-4}$
1000	$5.7 \times 10^{-4}$	$0.05 \times 10^{-4}$
1500	$8.2 \times 10^{-4}$	$0.35 \times 10^{-4}$
2000	$9.5 \times 10^{-4}$	$0.82 \times 10^{-4}$
2500	$1.3 \times 10^{-3}$	$0.09 \times 10^{-3}$
3000	$1.3 \times 10^{-3}$	$0.17 \times 10^{-3}$
3500	$1.1 \times 10^{-3}$	$0.10 \times 10^{-3}$

40°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$0.12 \times 10^{-3}$	$0.02 \times 10^{-3}$
1500	$1.6 \times 10^{-3}$	$0.13 \times 10^{-3}$
2000	$2.3 \times 10^{-3}$	$0.16 \times 10^{-3}$
2500	$2.6 \times 10^{-3}$	$0.16 \times 10^{-3}$
3000	$3.8 \times 10^{-3}$	$0.25 \times 10^{-3}$

50°C

pressure (kgcm <sup>-2</sup> )	<i>k</i> (l/mol·h)	error
1	$0.33 \times 10^{-3}$	$0.08 \times 10^{-3}$
1500	$5.0 \times 10^{-3}$	$0.81 \times 10^{-3}$
2000	$5.9 \times 10^{-3}$	$1.50 \times 10^{-3}$
2500	$7.8 \times 10^{-3}$	$0.29 \times 10^{-3}$
3000	$10 \times 10^{-3}$	$0.97 \times 10^{-3}$